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UNIVERSITI TUN HUSSEIN ONN MALAYSIA

**FINAL EXAMINATION
SEMESTER II
SESSION 2018/2019**

COURSE NAME : CHEMICAL REACTION ENGINEERING
COURSE CODE : DAK 32203
PROGRAMME CODE : DAK
EXAMINATION DATE : JUNE / JULY 2019
DURATION : 3 HOURS
INSTRUCTION : ANSWERS **TWO (2)** QUESTIONS
IN SECTION A AND **TWO (2)** QUESTIONS
IN SECTION B

THIS QUESTION PAPER CONSISTS OF NINE (9) PAGES

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SECTION A

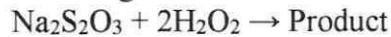
- Q1 (a) Chemical reaction engineering is virtually the heart of every chemical process.
- (i) State **two (2)** importance of learning chemical reaction engineering. (4 marks)
 - (ii) State **two (2)** parameters affecting the value of reaction rate, $-r_A$. (2 marks)
 - (iii) List all the units involved in the reaction rate, r_i . (3 marks)
 - (iv) Explain the differences between batch reactor and CSTR in terms of molar flow rate. (4 marks)
- (b) Methane gas can burn easily to produce hot flames, which can be used to boil water or cook. The combustion takes place in a 0.95 m diameter of cylindrical chamber. If this reaction consumes 1.8 kg/s of methane at a rate of $100 \text{ mol CH}_4/(\text{m}^3 \cdot \text{sec})$, find the reactor length. The combustion equation for methane is $\text{CH}_4 + 2\text{O}_2 \rightarrow \text{CO}_2 + 2\text{H}_2\text{O}$. [Molecular weight for C = 12 g/mol, H = 1 g/mol] (6 marks)
- (c) State **one (1)** disadvantage for each reactor below.
- (i) Batch reactor
 - (ii) CSTR
 - (iii) PFR
- (6 marks)

- Q2** (a) Iron react with oxygen gas to form iron (III) oxide, $4\text{Fe} + 3\text{O}_2 \rightarrow 2\text{Fe}_2\text{O}_3$
- (i) Express an equation to show relationship between $-r_A$ and $+r_C$. (2 marks)
 - (ii) Show the rate of iron being consumed, in $\text{mol.L}^{-1}\text{s}^{-1}$ if Fe_2O_3 was formed at a rate of $81.5 \text{ g.L}^{-1}\text{s}^{-1}$. (2 marks)
 - (iii) State the value of N_{A0} (in mole) if initially there are 15.6 grams of O_2 used in the reaction. [$\text{Fe} = 55.8 \text{ gram/mol}$, $\text{O} = 16 \text{ gram/mol}$] (3 marks)
- (b) The combustion of hydrogen, $2\text{H}_2 + \text{O}_2 \rightarrow 2\text{H}_2\text{O}$ is carried out with the desired conversion of $X = 70\%$.
- (i) Compare CSTR and PFR volumes when the molar flow rate is 5 mole/sec. Use the reaction data in **Table 1**. (6 marks)
 - (ii) State type of reactor to be used if the reaction requires good temperature control and must be carried out in the liquid phase. (2 marks)
- (c) Reactors can be run in series so that the total conversion process is split into few stages.
- (i) Calculate total reactor volume for a series of reactors with the sequence of CSTR \rightarrow PFR \rightarrow CSTR, with conversions of $20\% \rightarrow 25\% \rightarrow 30\%$. F_{A0} is 30 mol/s. Use the same reaction data in **Table 1**. (8 marks)
 - (ii) Explain why batch reactor cannot be used in the series reactor. (2 marks)

SECTION B

- Q3** (a) Reaction rate law is also known as “rate equation” or “rate law”.
- (i) Write the rate law for the reaction of $\text{Cu} + 2\text{AgNO}_3 \rightarrow 2\text{Ag} + \text{Cu}(\text{NO}_3)_2$.
(2 marks)
- (ii) Write the non-elementary rate law equation and the reversible rate law equation for the reaction in **Q3 (a)(i)**.
(4 marks)
- (iii) Explain *the order of reaction* and *the overall order of reaction* based on the reaction in **Q3 (a)(i)**.
(4 marks)
- (b) Write a simplified chemical equation for each case below using the alphabetical symbol (eg: A, B, C, etc).
- (i) Unimolecular reaction.
(ii) Bimolecular reaction.
(iii) Termolecular reaction.
(6 marks)
- (c) The neutralization reaction below is carried out in a liquid phase, steady state CSTR.
$$3\text{NH}_4\text{OH} + \text{H}_3\text{PO}_4 \rightarrow (\text{NH}_4)_3\text{PO}_4 + 3\text{H}_2\text{O}$$
- (i) Copy and complete **Table 2** in your answer script, assuming that the inert component in the reaction is Nitrogen.
(7 marks)
- (ii) State **one (1)** use of the stoichiometric table.
(2 marks)

- Q4** (a) The liquid phase reaction of sodium thiosulfate and hydrogen peroxide is carried out in a **constant-volume** batch reactor as given below.



$$k = 5.73 \times 10^{10} \exp(-E/RT)$$

$$T = 30^\circ\text{C}$$

$$R = 8.314 \text{ J/mol.K}$$

$$E = 76.48 \text{ kJ/mol A}$$

$$C_{A0} = 100 \text{ mol/m}^3$$

$$C_{B0} = 200 \text{ mol/m}^3$$

- (i) Calculate the value of k . (2 marks)
- (ii) Write the rate law equation, when the actual reaction order is first order for component A and first order for component B. (2 marks)
- (iii) Compare reaction times, t for 50% and 80% conversions. (6 marks)
- (b) You are now tasked to design the reactor volume based on the data given in **Q4 (a)**.
- (i) Construct a table of conversion (X) versus rate law ($-r_A$) for 0%, 50% and 80% conversion based on rate law equation in **Q4 (a)(ii)**. (4 marks)
- (ii) Compare reactor volume, V for 50% and 80% conversions if $N_{A0} = 100$ mole. (4 marks)
- (c) The reaction **Q4 (a)** is then tested in a CSTR with the initial volumetric flow rate, v_0 of 0.5 Liter/s and 70% conversion. If the volumetric flow rate is increased two times from its original value, show the changes in the conversion value. Assume that first order for component A and zero order for component B. (7 marks)

- Q5** (a) Series and parallel reaction can be considered to be chosen for a complex reaction.
- (i) Define parallel reaction and series reaction. (4 marks)
- (ii) Write **TWO (2)** set of reactions to differentiate between multiple and independent reaction. (4 marks)
- (b) The aim of selecting a parallel reaction is always to obtain high desired product.
- (i) Write the reaction rate law for the parallel reaction below.

$$2A \xrightarrow{k_D} D$$

$$A \xrightarrow{k_U} U$$
 (3 marks)
- (ii) Explain **ONE (1)** method to maximize the desired product, D for the reaction in **Q5 (b)(i)**. (2 marks)
- (iii) State **ONE (1)** effect if the amount of undesired product, U is too high. (3 marks)
- (c) One of important variable for a series reaction is the reaction rate constant.
- (i) State which one of the series reactions below is more preferred.
 Reaction 1: $A \xrightarrow{k_1=10 \text{ sec}^{-1}} D \xrightarrow{k_2=2 \text{ sec}^{-1}} U$
 Reaction 2: $A \xrightarrow{k_1=3 \text{ sec}^{-1}} D \xrightarrow{k_2=7 \text{ sec}^{-1}} U$ (3 marks)
- (ii) Explain the effect on the reaction if the opposite answer in **Q5 (c)(i)** is chosen. (2 marks)
- (d) Write **TWO (2)** steps in the algorithm to solve complex, multiple reactions. (4 marks)

- Q6** (a) Catalyst have been used by the humankind for over 2000 years.
- (i) Define the term catalyst. (3 marks)
 - (ii) Name few examples of catalysts used in food industry. (4 marks)
- (b) Based on the statements below, state whether they are homogeneous or heterogeneous catalytic reaction.
- (i) Dehydrogenation process of liquid cyclohexane using platinum-on-alumina as the catalyst.
 - (ii) "Fisher esterification" process occurs when a liquid alcohol and liquid acid react to form ester, using sulphuric acid solution as a catalyst.
 - (iii) "Haber process" occurs when hydrogen gas and nitrogen gas react to form ammonia, using metal iron as a catalyst. (6 marks)
- (c) A catalytic reaction occurs mainly at the fluid-solid interface.
- (i) Explain porous catalyst, molecular sieves and monolithic. (6 marks)
 - (ii) State **THREE (3)** ways to deactivate a catalyst. (3 marks)
- (d) State the **THREE (3)** main steps in the catalytic reaction based on the **Figure Q6 (d)**. Take note that the lined surface on each image sequence below is the catalyst surface. (3 marks)

-END OF QUESTIONS -

FINAL EXAMINATION

SEMESTER/SESSION : SEMESTER II 2018/2019
 COURSE NAME : CHEMICAL REACTION ENGINEERING

PROGRAMME : DAK
 COURSE CODE : DAK 32203

Table 1

X	$-r_A (mol/m^3.s)$
0.00	3.9
0.20	3.5
0.45	2.6
0.70	1.1
0.75	1.23

Table 2

Species Name	Symbol	Molar Flow Rate, $F_i (mol/s)$		
		Initial (mol/s)	Change (mol/s)	Remaining (mol/s)
				$F_A =$
				$F_B =$
				$F_C =$
				$F_D =$

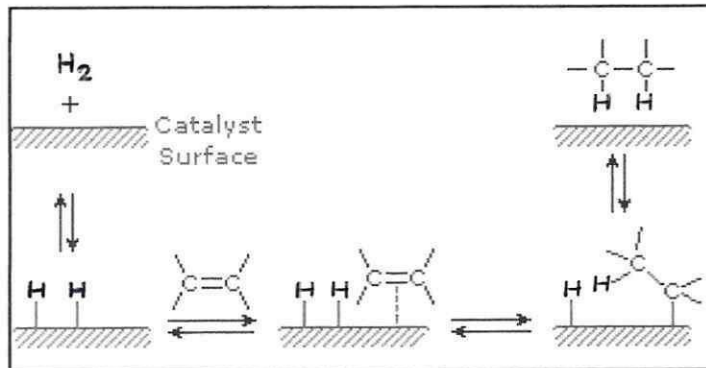


Figure Q6 (d)

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List of Formula

Batch reactor:
$$V = \frac{N_{A0}}{t} \int_{X(0)}^{X(t)} \frac{dX}{-r_A}$$

Batch reactor time:
$$t = C_{A0} \int_{X(0)}^{X(t)} \frac{dX}{-r_A}$$

CSTR:
$$V = \frac{F_{A0} X}{-r_A}$$

CSTR in series:
$$V = F_{A0}(X_1 - X_0) \div -r_A$$

PFR:
$$V = F_{A0} \int_{X(0)}^{X(t)} \frac{dX}{-r_A}$$

Simpson's trapezoidal rule (two-point rule),

$$\int_{X_0}^{X_1} f(X) dX = \frac{h}{2} [f(X_0) + f(X_1)]$$

Simpson's one third rule (three point rule),

$$\int_{X_0}^{X_2} f(X) dX = \frac{h}{6} [f(X_0) + 4f(X_1) + f(X_2)]$$

Where, $f(X_0)$ is the value of $1 / (-r_A)$ at point X_0 and h is the distance between conversion points.

$$C_{A0} = N_{A0} \div V$$

$$k = A e^{\frac{-E}{RT}}$$

$$C_A = C_{A0} (1 - X)$$

$$F_A = F_{A0} (1 - X)$$

$$\int \frac{1}{(1 - X)^2} dX = \frac{1}{(1 - X)}$$

$$Da = \frac{-r_A V}{F_{A0}}$$

$$F_{A0} = v_0 C_{A0}$$